



FAHRENHEIT

Alumino-phosphate coatings: From lab-scale adsorption experiments to the design of adsorption chiller heat-exchangers

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Who we are

2002 Founded as SorTech AG as spin-off from Fraunhofer ISE

2017 Rebranding into Fahrenheit GmbH

- Development and production of adsorption chillers
- Development of adsorption applications

35 Employees in Munich (sales, head office)
and Halle/Saale (R&D and production)

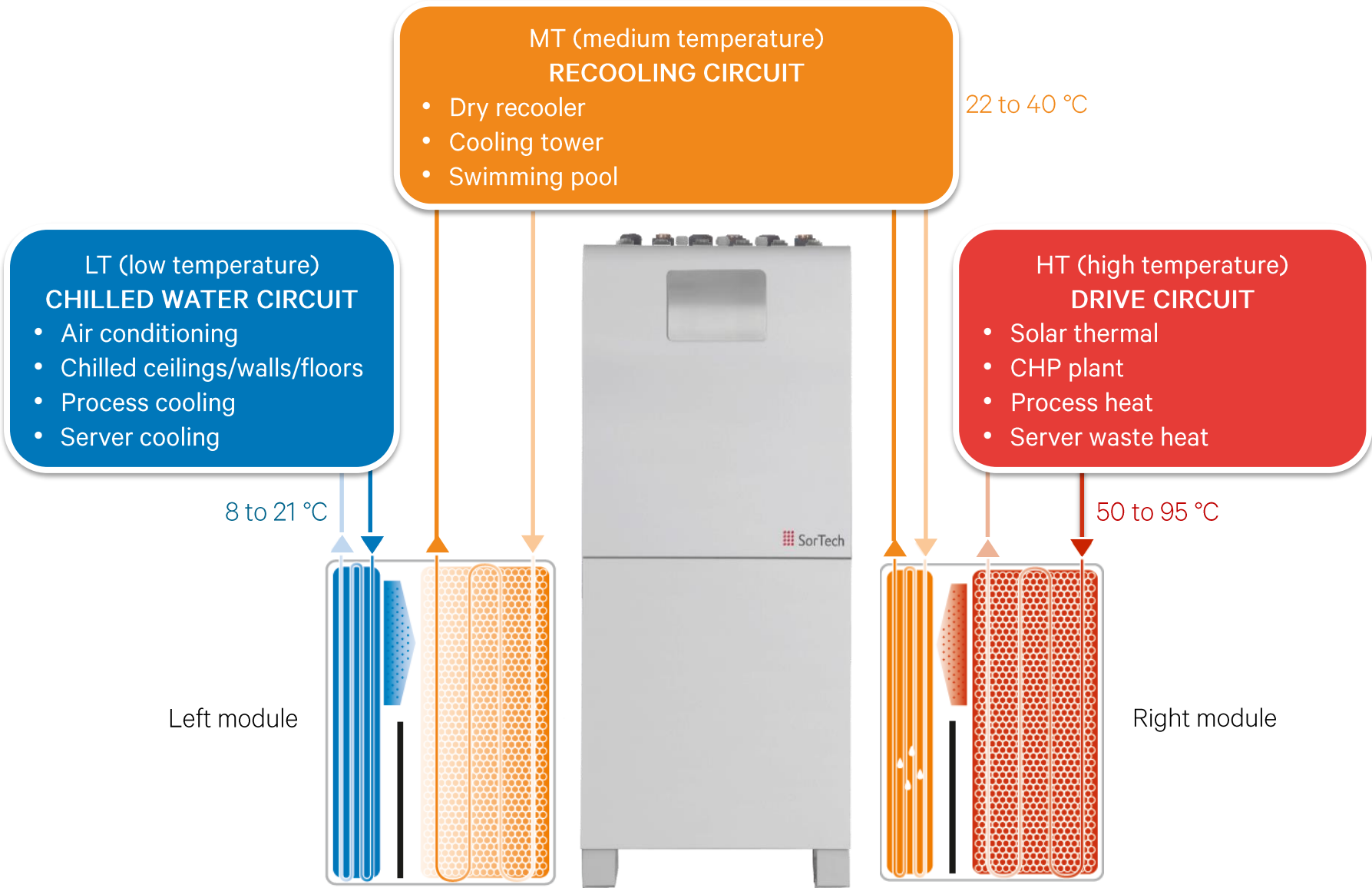
>20 Patents granted

>600 Systems installed (Germany, Europe, overseas)

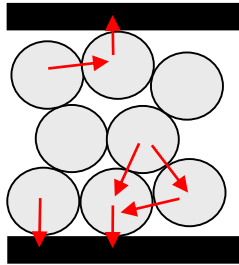
10 to 750 kW system cooling power



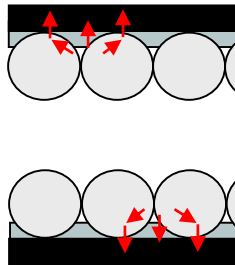
Technical implementation of an adsorption chiller



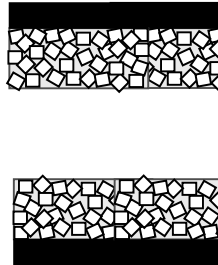
Rapid heat transfer is essential for adsorption cooling



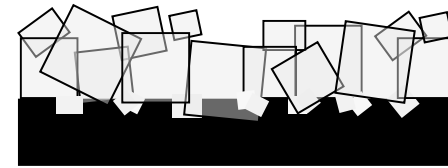
fixed bed



fixed monolayer



binder coating



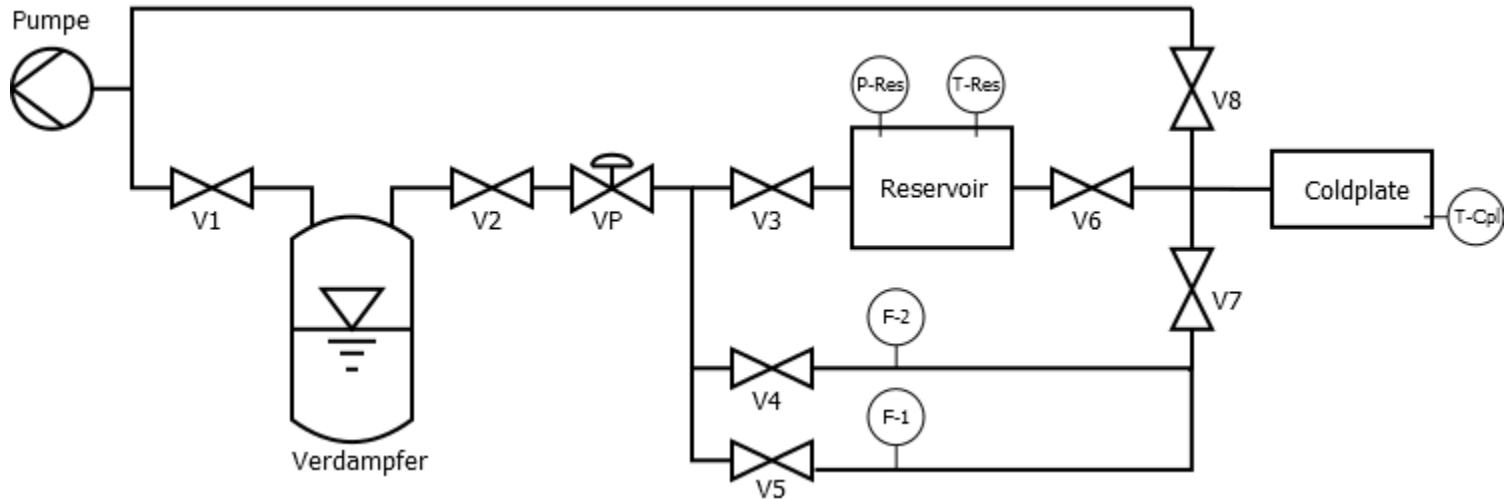
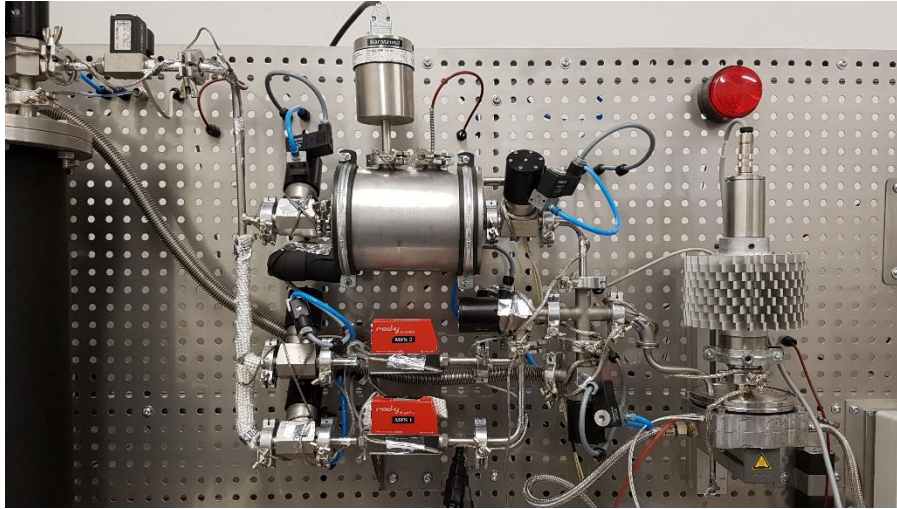
partial support transformation (PST)

Increasing heat transfer
Increasing adsorption rate
Increasing cooling power

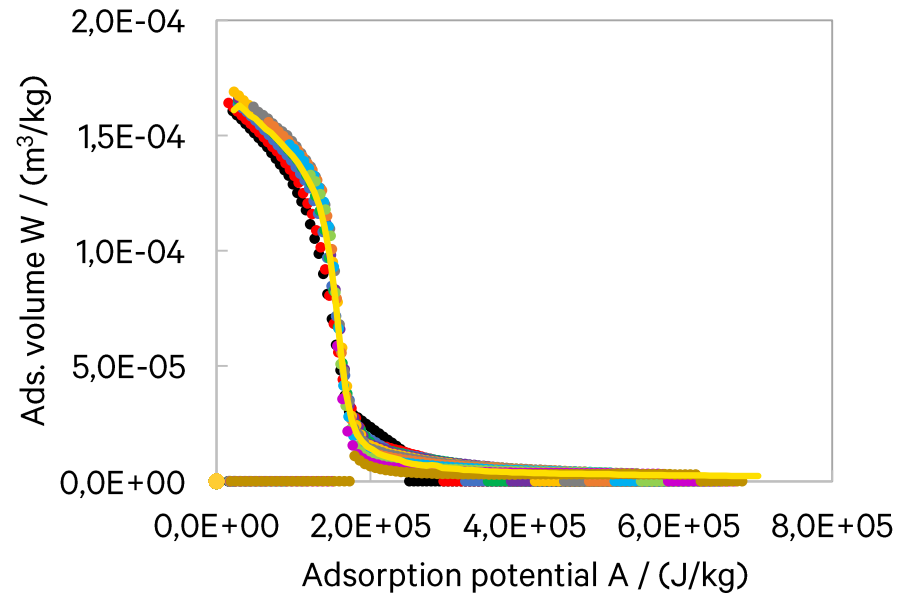
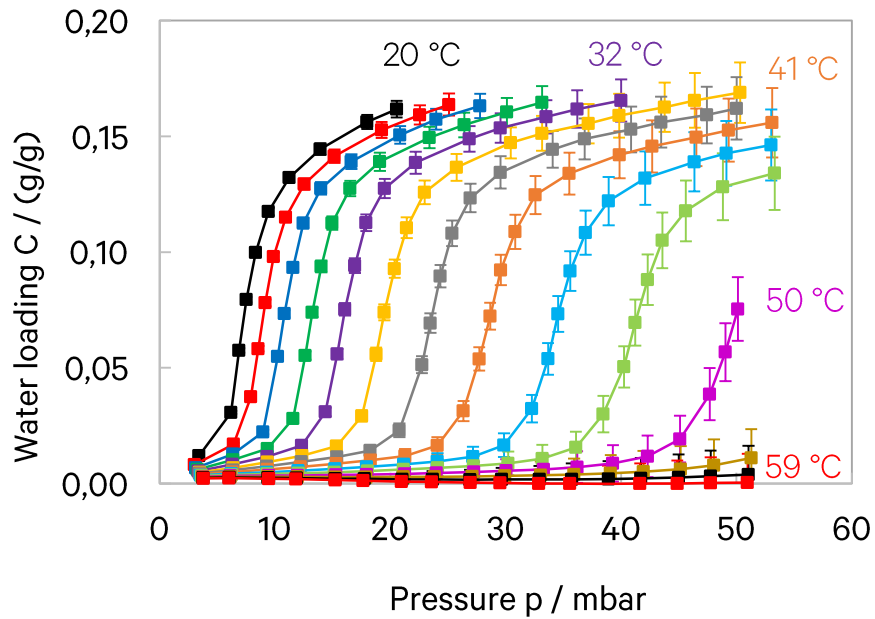
Performance assessment on different scales

Scale	Experiments	Information on
Lab	Isothermal static adsorption, Isothermal dynamic adsorption	p , T operating window of the adsorbent, Influence of layer thickness and morphology
Heat exchanger	Non-isothermal dynamic adsorption	Interaction of adsorption and heat transfer
Module	Performance assessment	Interaction of condenser and adsorber
Chiller	Performance assessment	Interaction of modules with hydraulics

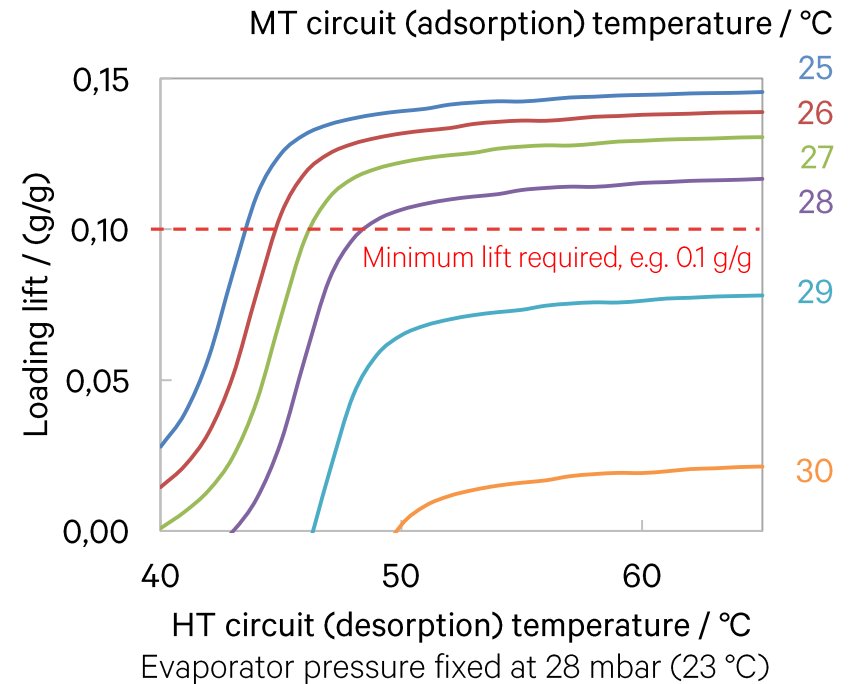
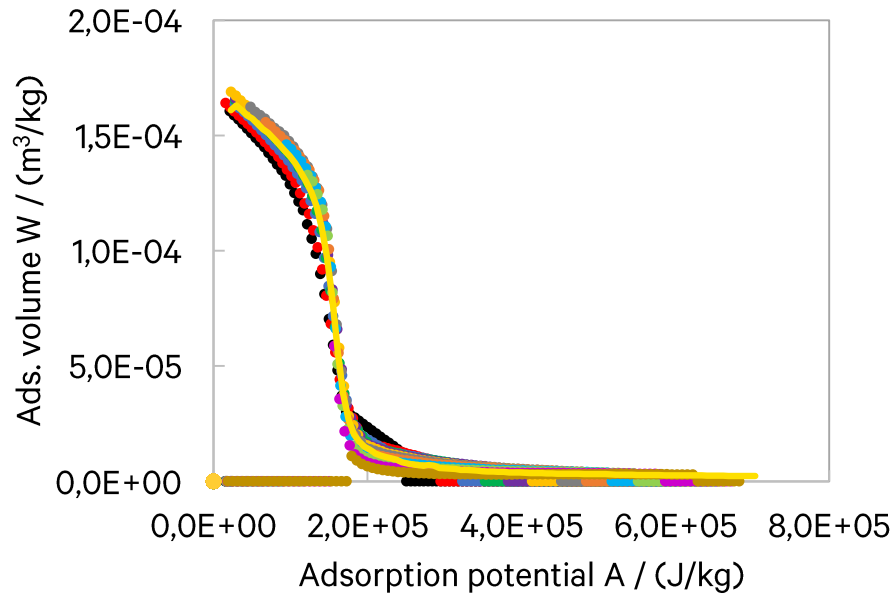
Lab-scale characterisation setup



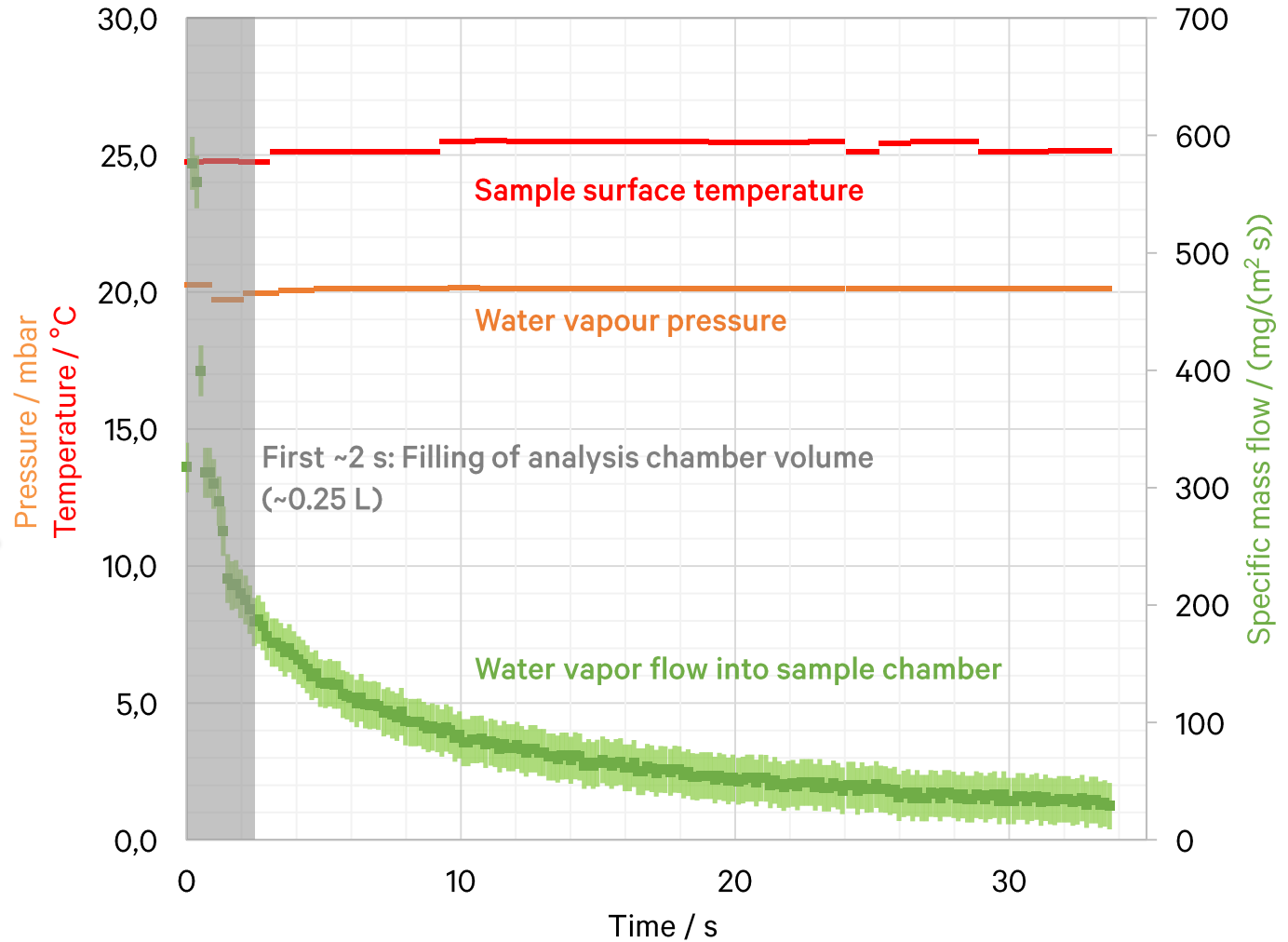
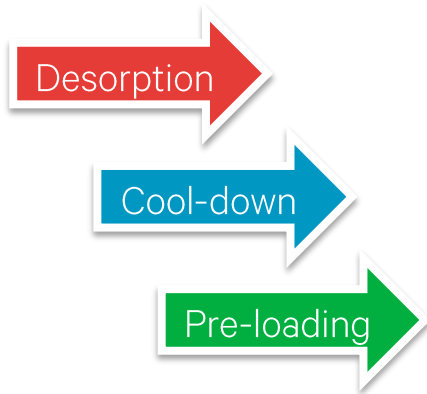
Calculation of the characteristic curve



Assessment of the operation window from the characteristic curve



Isothermal pressure jump experiment



Identification of a suitable kinetic model

Elovich's equation

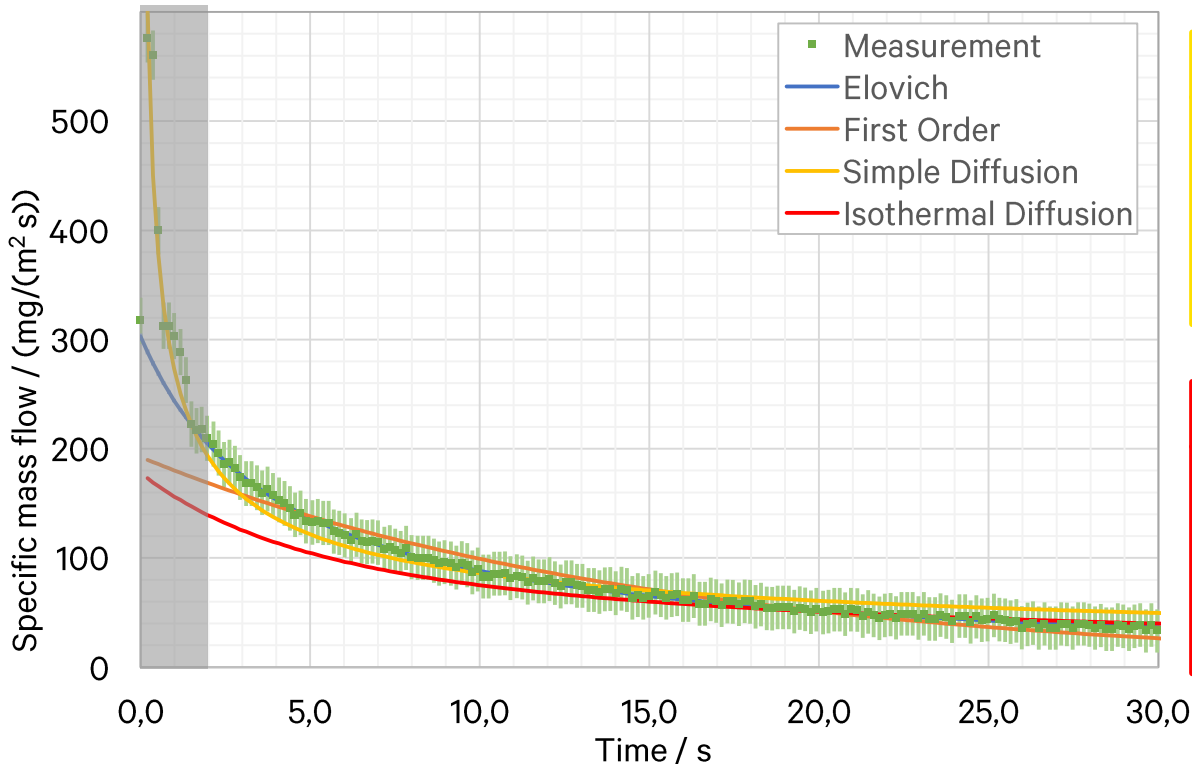
$$C(t) = \beta \ln \left(\exp \left(\frac{C_0}{\beta} \right) + \frac{r_0 t}{\beta} \right)$$

$$r(t) = r_0 \exp \left(-\frac{C(t)}{\beta} \right) \equiv \frac{\beta r_0}{\beta \exp \left(\frac{C_0}{\beta} \right) + r_0 t}$$

First order

$$C(t) = C_{eq} \left(1 - \exp \left(-\frac{t}{\tau} \right) \right)$$

$$r(t) = \frac{C_{eq}}{\tau} \exp \left(-\frac{t}{\tau} \right)$$



Simple diffusion

$$C(t) = C_0 + (C_{eq} - C_0) \sqrt{ut}$$

$$r(t) = \frac{(C_{eq} - C_0)}{2} \sqrt{\frac{u}{t}}$$

Isothermal diffusion

$$C(t) = C_{eq} \left(1 - \frac{6}{\pi^2} \sum \frac{1}{n^2} \exp \left(-\frac{n^2 \pi^2 D t}{r^2} \right) \right)$$

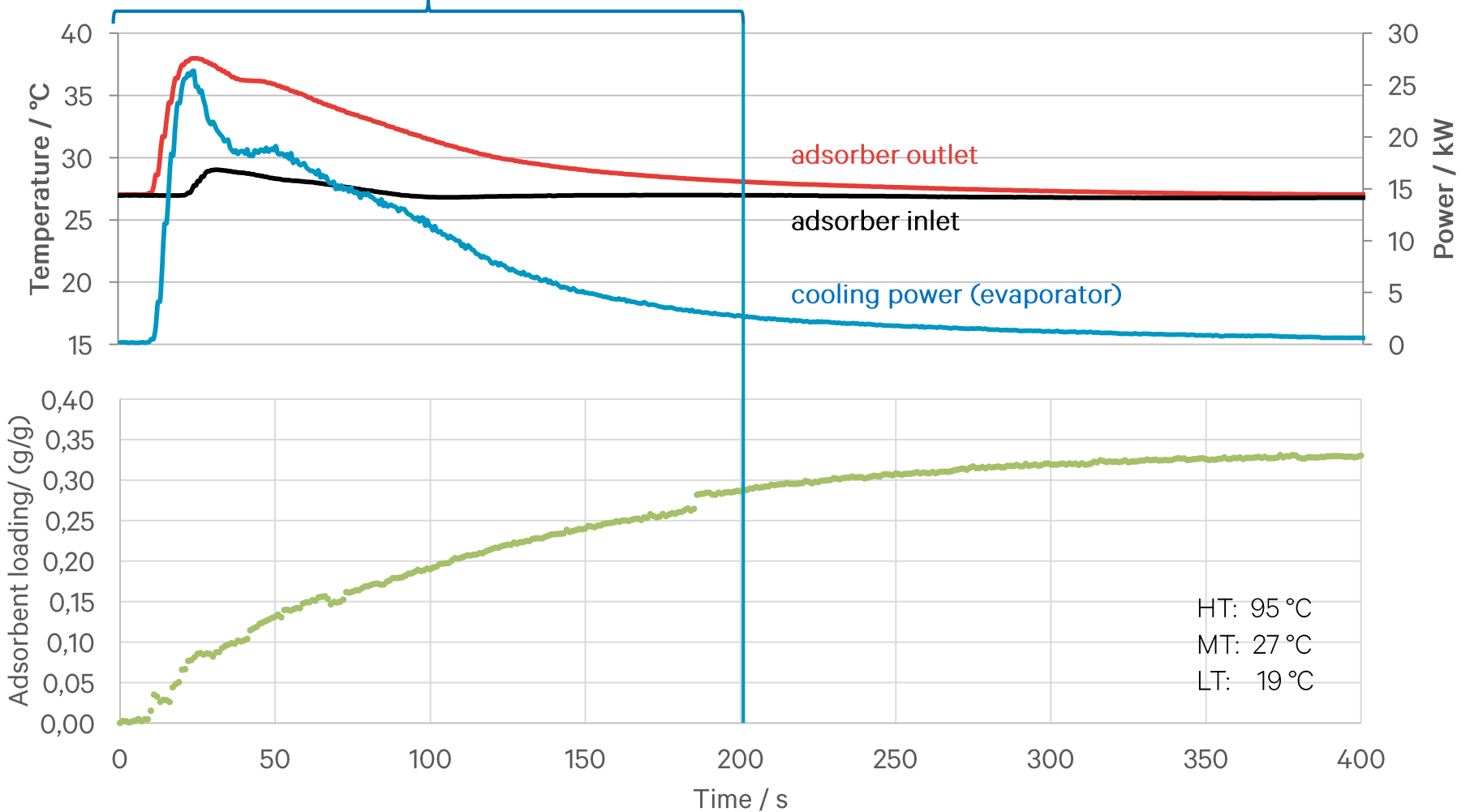
$$r(t) = \frac{dC(t)}{dt}$$

Heat exchanger scale setup

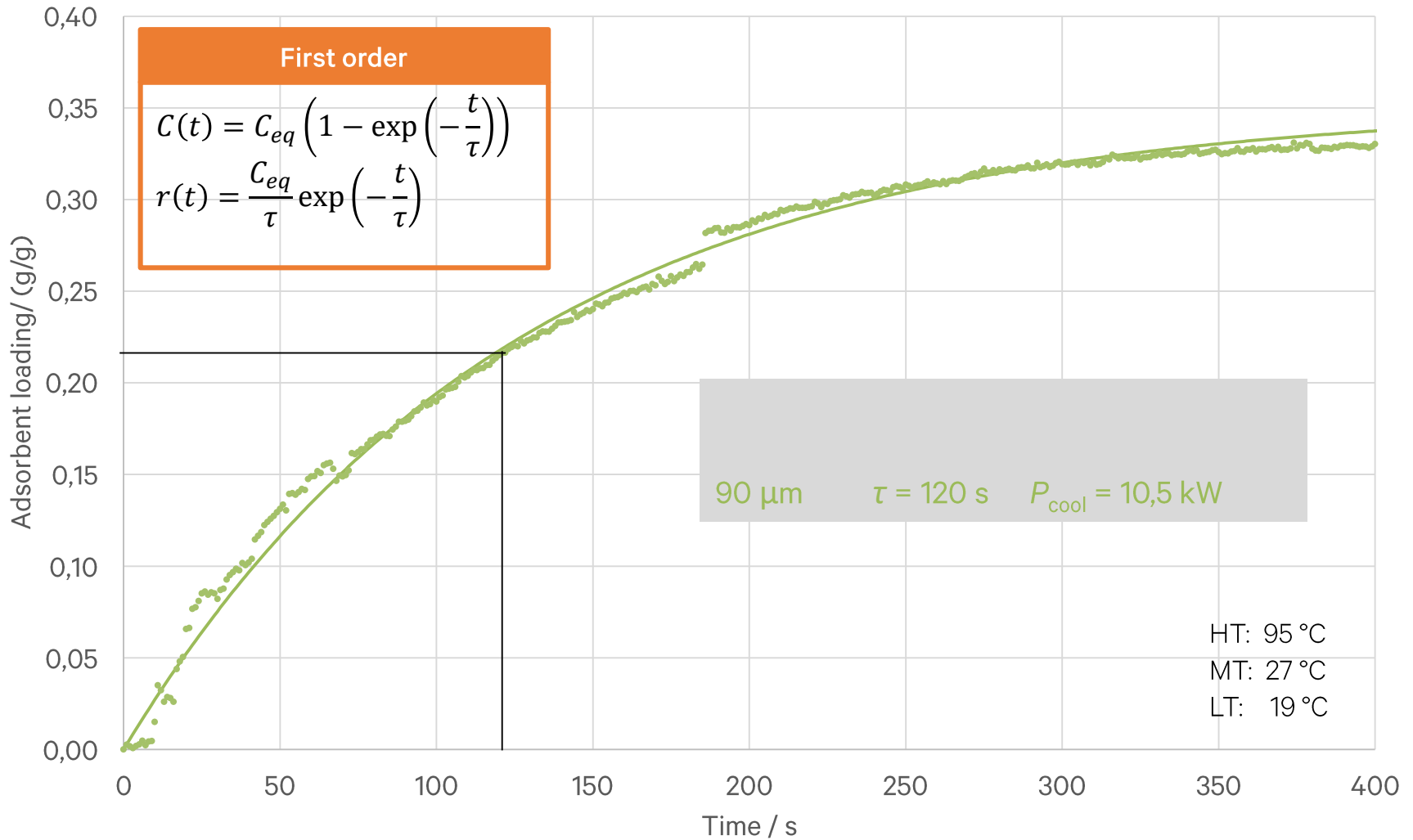


Non-isothermal adsorption experiment

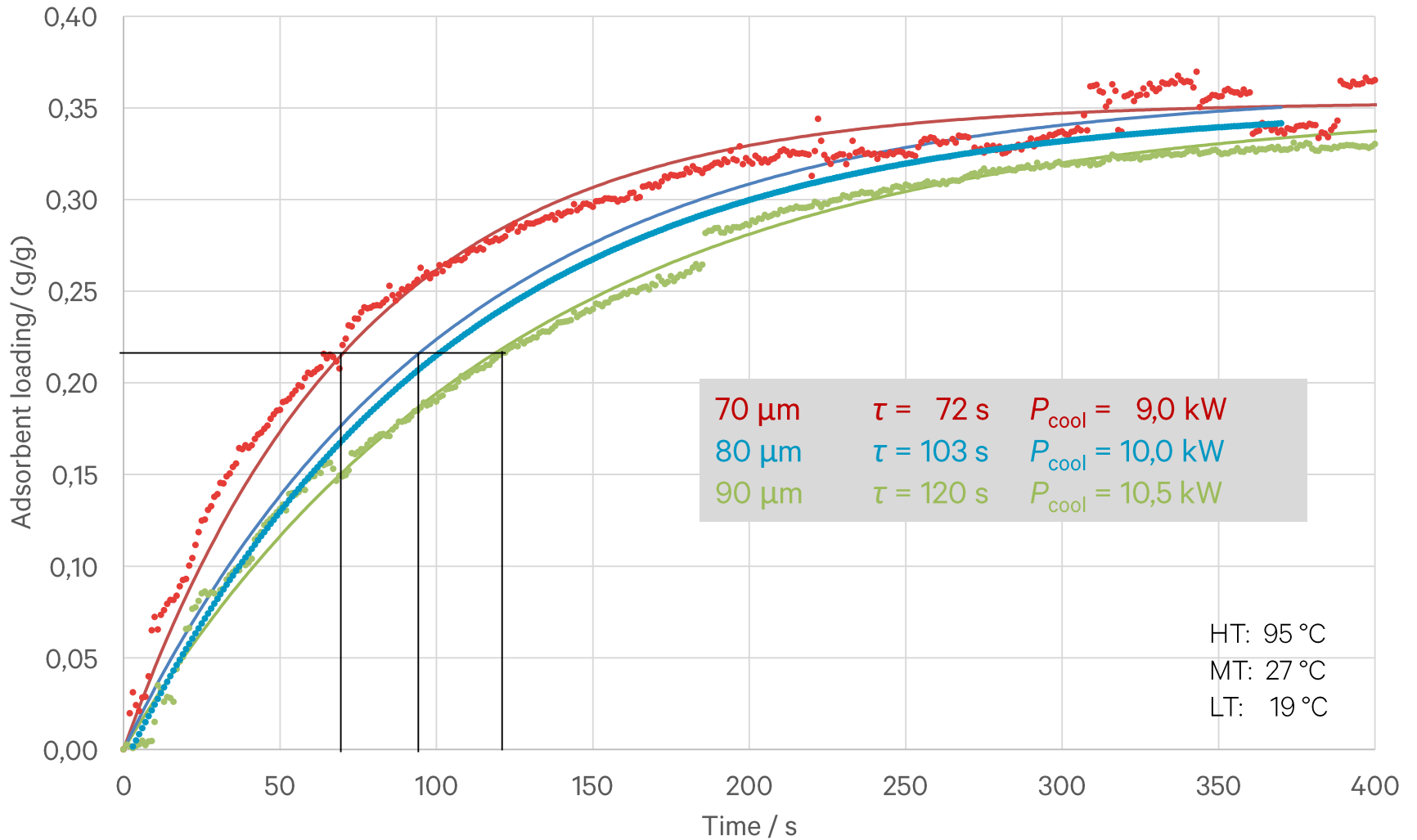
Mean cooling power (200 s): 10.5 kW



Non-isothermal adsorption experiment



Influence of adsorbent-layer thickness on cooling power



Summary and Outlook

- Rapid sorption process is essential for adsorption chillers (cooling power!)
- Static and dynamic sorption experiments on different scales throughout the development process

Outlook

- Mathematical adsorber performance prediction to reduce development time and cost





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